

Thermochemical Heat Storage for Baseload Concentrated Solar Power Generation

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Outline:

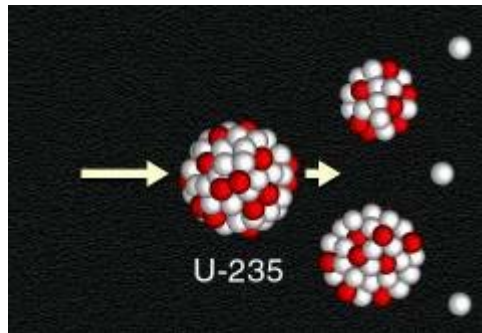
- Solar Energy Storage in Solar-thermal (Tower)Power Plants (STPPs)
- ThermoChemical Storage (TCS) principles
- Demonstration: the Restructure Storage
- Some new ideas on redox-oxide-based porous ceramics for TCS and sulfur based TCS in STPPs
- Conclusions, current and future work



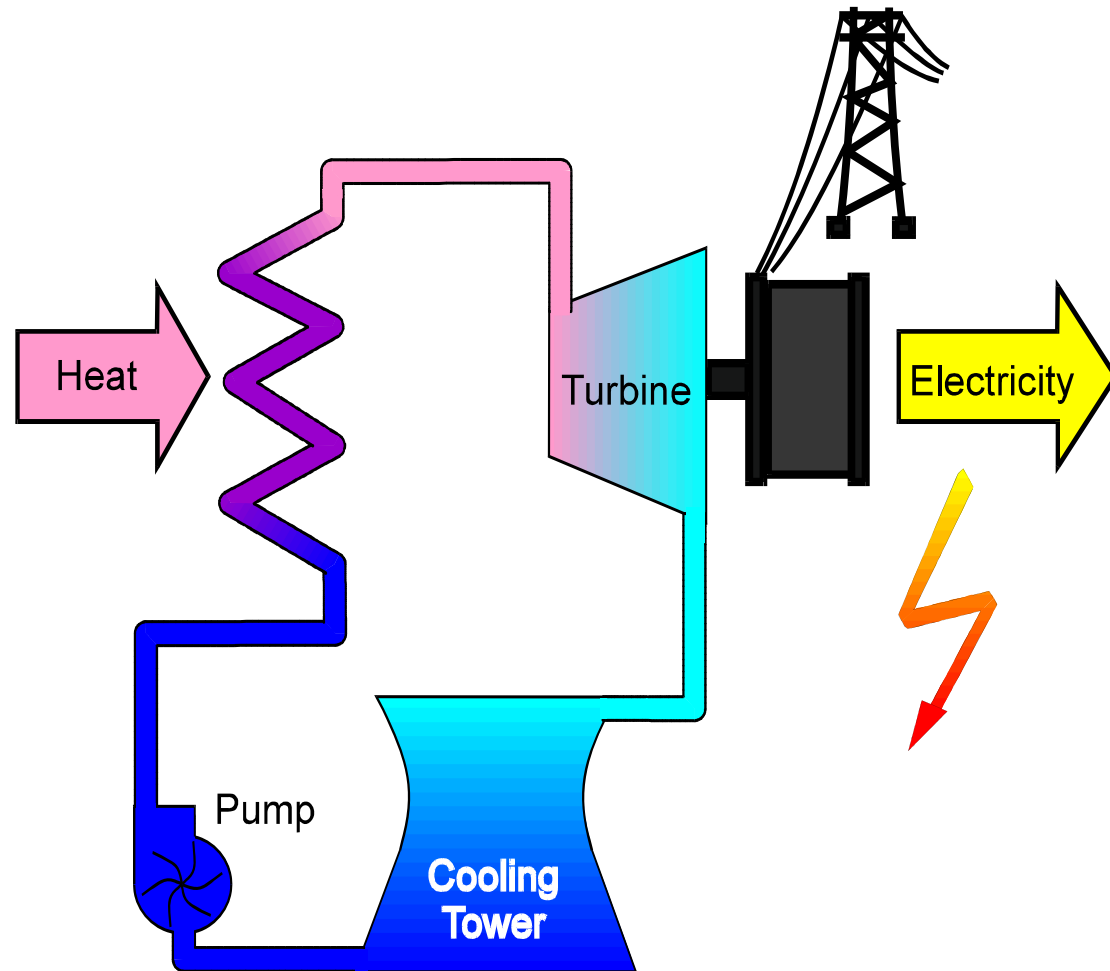
DLR's Solar Tower, Jülich, Germany



What is CSP ?



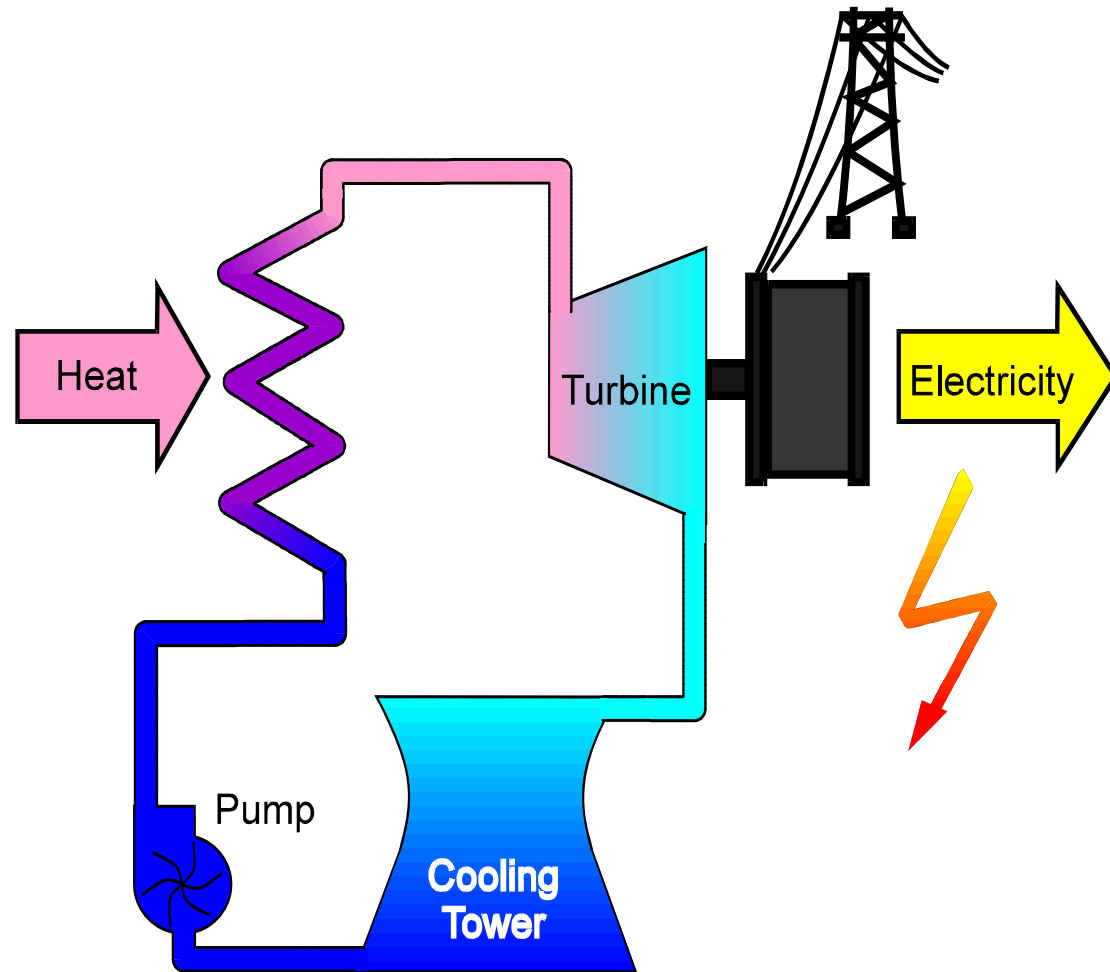
Conventional power plants



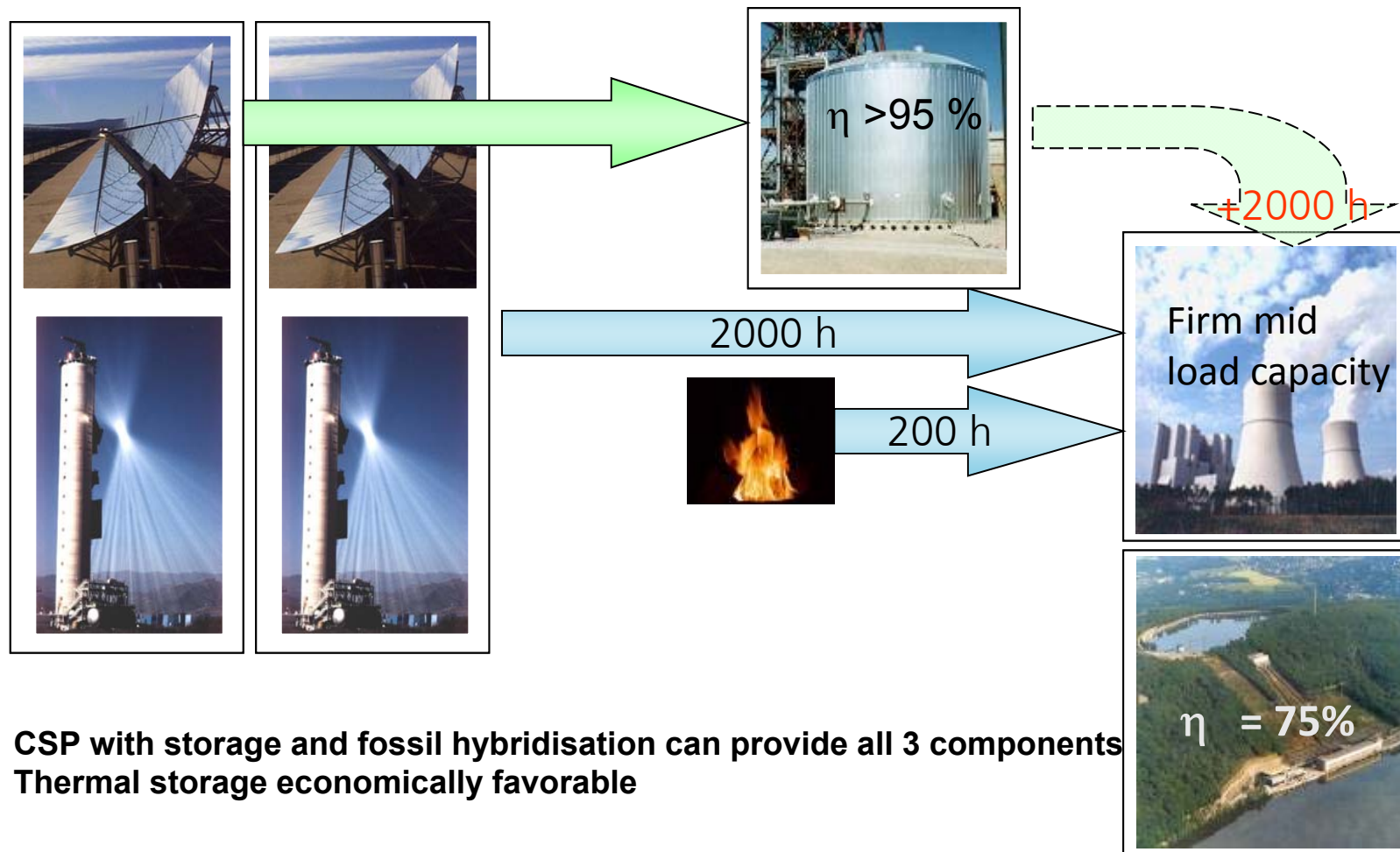
What is CSP ?



Solar thermal power plants



Thermal Storage vs. Electric Storage



CSP with storage and fossil hybridisation can provide all 3 components
Thermal storage economically favorable



Thermochemical heat storage can provide very high energy storage densities

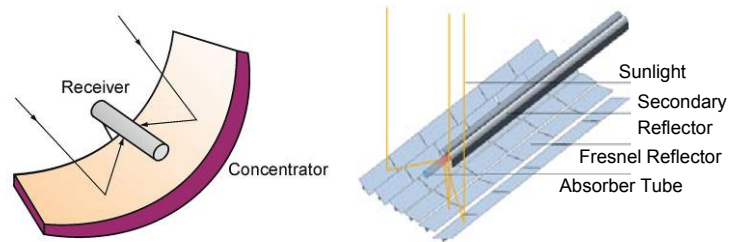
Technology	Energy Density (kJ/kg)
Gasoline	45000
Sulfur	12500
Cobalt Oxide	850
Molten Salt (Phase Change)	230
Molten Salt (Sensible)	155
Lithium Ion Battery	580
Elevated water Dam (100m)	1

- **High energy densities with low storage cost**
- **Ambient and long term storage**
- **Transportability**

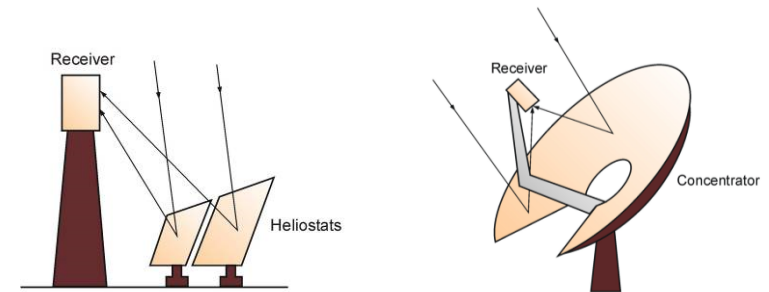


Concentrator Options for CSP Technology

line concentrators



point concentrators



Technology	Peak solar to electricity conversion efficiency	Annual solar-to-electricity efficiency	Water consumption, for wet/dry cooling (m ³ /MWh)	Land use (m ² /MWh/a)
Parabolic troughs	23-27%	15-16%	3-4 / 0.2	6-8
Linear Fresnel systems	18-22%	8-10%	3-4 / 0.2	4-6
Towers (central receiver systems)	20-27%	15-22%	3-4 / 0.2	8-12



Solar Towers

PS 10



Crescent Dunes



Ivanpah Solar



Torresol



PSA SSPS



PSA CESA-1



On the Web:

<http://www.ivanpahsolar.com/>

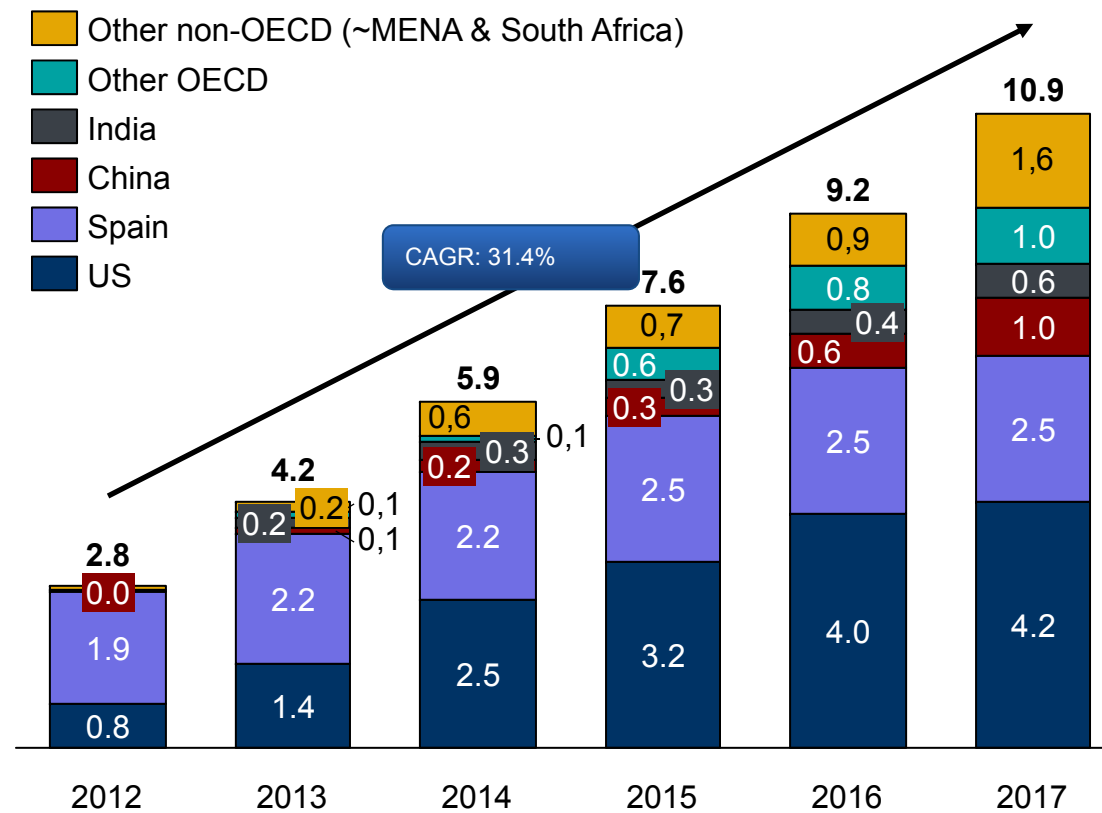
<http://www.psa.es/webeng/index.php>

<http://www.torresolenergy.com/TORRESOL/home/en>

<http://www.solarreserve.com/en/global-projects/csp/crescent-dunes>

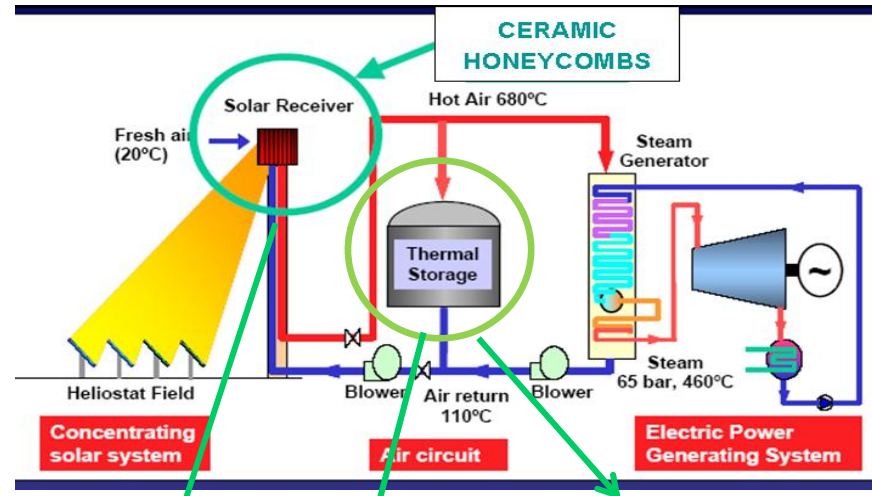
http://www.abengoasolar.com/web/en/plantas_solares/plantas_para_terceros/espana/

CSP Market Development according to IEA



Air-operated CSP Plants (Solar Tower Jülich/STJ)

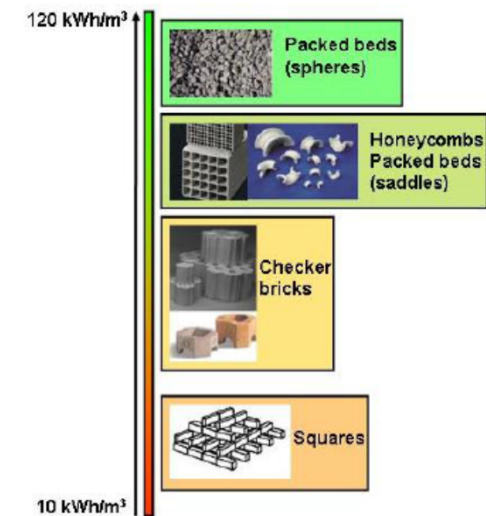
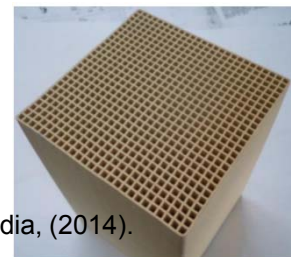
- HTF: Air at atmospheric pressure, heated up to about 700°C and then powering a steam generator.
- Sensible heat storage : TES by temperature increase ($cp \Delta T$)



Storage design specifications	
Inlet Temperature (Charge/ Discharge)	680 °C / 120 °C
Outlet temperature (Charge/Discharge)	680-640 °C 120-150 °C
Charge mass flow	9.4 kg/s
Discharge heat rate	5.7 MWth
Full load discharge period	1.5 h
Pressure loss	< 1500 Pa

Table 2 Inventory

Honeycombs	60 × 60 cells
Brick dimensions	150 × 150 × 150 (mm)
Material	Alumina porcelain (C130)
Bulk density	2700 kg/m ³
Specific heat capacity	0.88 kJ/(kg K)
Thermal conductivity	2.1 W/(m K)
Heating surface	1180 m ² /m ³
Free cross section	69%



S. Zunft, et al.:SolarPACES, (2009); (2010); JSEE (2011); Energy Procedia, (2014).



ThermoChemical Storage (TCS)

Reaction	No	ΔH (kJ/mol _{react})	T (°C)
$\text{NH}_3 + \Delta H \leftrightarrow \frac{1}{2} \text{N}_2 + \frac{3}{2} \text{H}_2$	(1)	49	593
$\text{Ca(OH)}_2 + \Delta H \leftrightarrow \text{CaO} + \text{H}_2\text{O}$	(2)	100	521
$\text{CaCO}_3 + \Delta H \leftrightarrow \text{CaO} + \text{CO}_2$	(3)	167	896
$2 \text{Co}_3\text{O}_4 + \Delta H \rightarrow 6 \text{CoO} + \text{O}_2$	(4)	202	890

- **HSM:** NH_3 , Solids: Ca(OH)_2 , CaCO_3 , Co_3O_4 respectively. **HTF: ?**
- Among the gas-solid reactions, mentioned above “... Oxide based systems have an advantage because **air is used as both the heat transfer fluid and the reactant** which eliminates the requirements to either store CO_2 or to evaporate water in the other TCS alternatives...”.



From TES with sensible heat to TCS with redox oxides

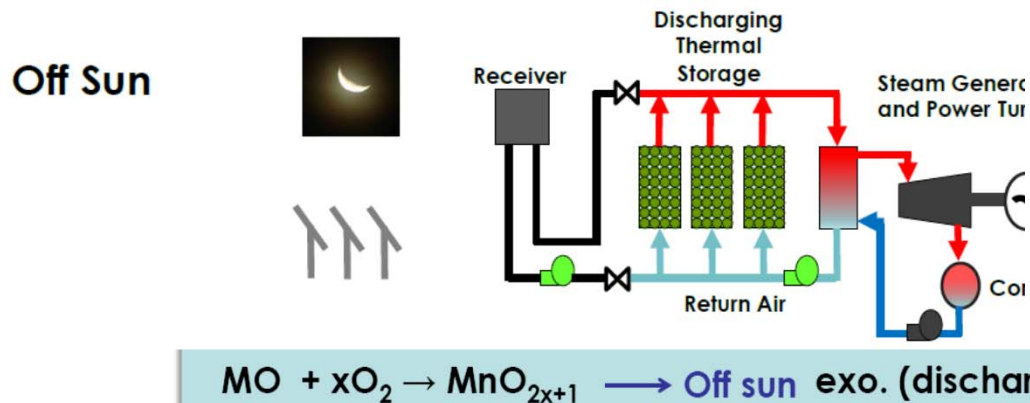
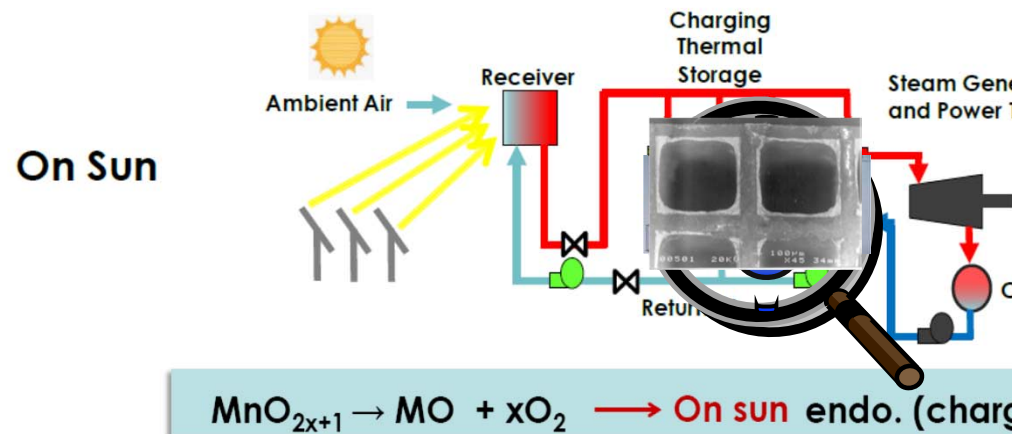


Table 2.1
Metal Oxide Systems Applicable to TES Based on Thermodynamics Considerations

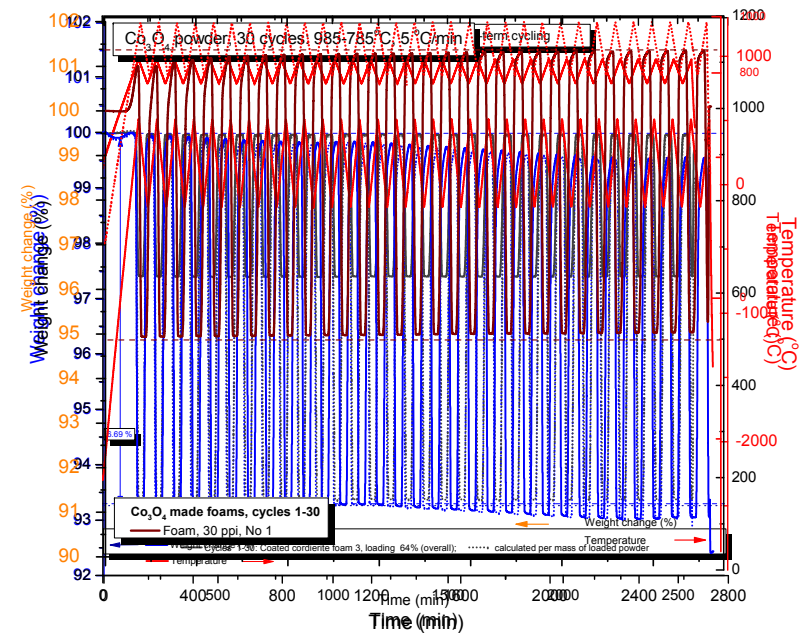
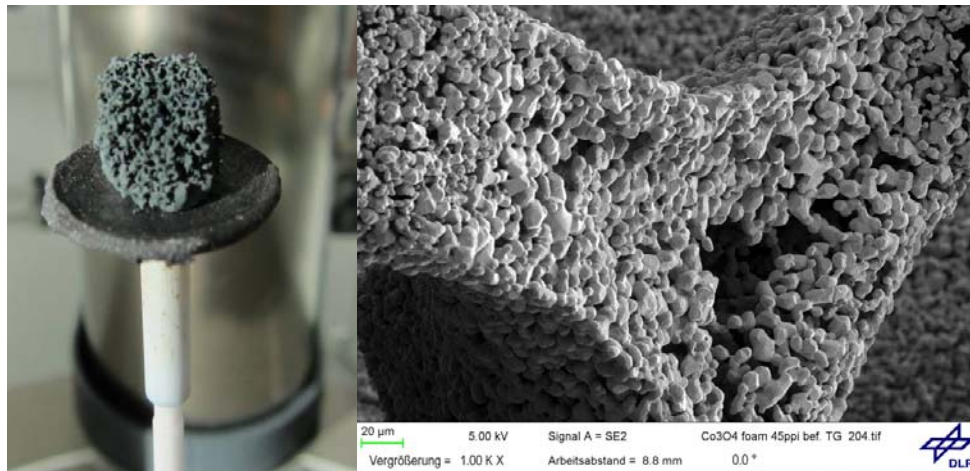
Reaction	Temperature (°C)	ΔH (kJ/mole oxide)	Storage Density (kJ/kg)
$\text{Cr}_5\text{O}_{12} \rightarrow 2.5\text{Cr}_2\text{O}_3 + 2.25\text{O}_2$	110	126.0	279
$2\text{Li}_2\text{O}_2 \rightarrow 2\text{Li}_2\text{O} + \text{O}_2$	150	68.2	1483
$2\text{Mg}_2\text{O} \rightarrow 2\text{MgO} + \text{O}_2$	205	21.8	505
$2\text{PbO}_2 \rightarrow 2\text{PbO} + \text{O}_2$	405	62.8	262
$2\text{PbO}_2 \rightarrow 2\text{PbO} + \text{O}_2$	420	62.8	277
$2\text{Sb}_2\text{O}_3 \rightarrow 2\text{Sb}_2\text{O}_4 + \text{O}_2$	515	92.5	286
$4\text{MnO}_2 \rightarrow 2\text{Mn}_2\text{O}_3 + \text{O}_2$	530	41.8	481
$6\text{UO}_3 \rightarrow 6\text{U}_3\text{O}_8 + \text{O}_2$	670	35.2	123
$2\text{BaO}_2 \rightarrow 2\text{BaO} + \text{O}_2$	885	72.5	474
$2\text{Co}_3\text{O}_4 \rightarrow 6\text{CoO} + \text{O}_2$	890	202.5	844
$\text{Rh}_2\text{O}_3 \rightarrow \text{Rh}_2\text{O} + \text{O}_2$	970	249.2	981
$6\text{Mn}_2\text{O}_3 \rightarrow 4\text{Mn}_3\text{O}_4 + \text{O}_2$	1000	31.9	202
$4\text{CuO} \rightarrow 2\text{Cu}_2\text{O} + \text{O}_2$	1120	64.5	811
$6\text{Fe}_2\text{O}_3 \rightarrow 4\text{Fe}_3\text{O}_4 + \text{O}_2$	1400	79.2	496
$2\text{V}_2\text{O}_3 \rightarrow 2\text{V}_2\text{O}_4 + \text{O}_2$	1560	180.7	993
$2\text{Mn}_3\text{O}_4 \rightarrow 6\text{MnO} + \text{O}_2$	1700	194.6	850

General Atomics: GA-C27137: THERMOCHEMICAL HEAT STORAGE FOR CONCENTRATED SOLAR POWER THERMOCHEMICAL SYSTEM REACTOR DESIGN FOR THERMAL ENERGY STORAGE ; Phase II Final Report, 2011



Co₃O₄/CoO: TGA

- Co₃O₄ can operate in a quantitative, cyclic and fully reversible reduction/oxidation mode within 800-1000°C (950°C).
- As powder, coated on honeycombs/foams or shaped in foams.

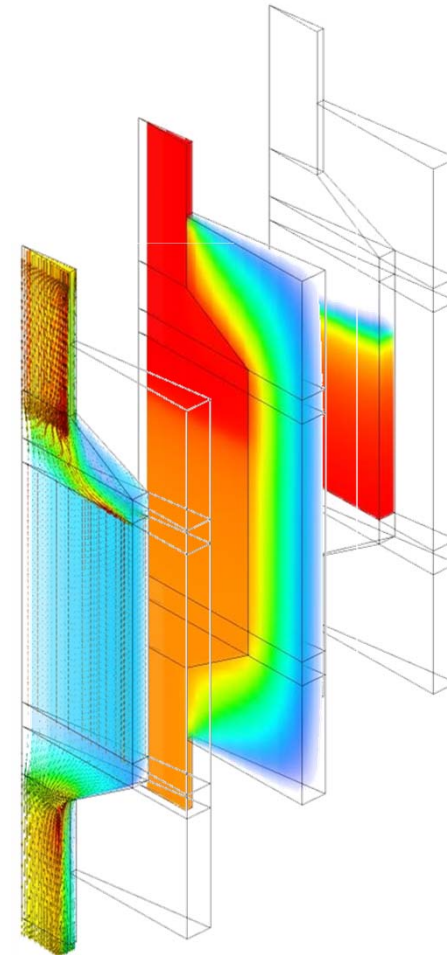


Agrafiotis, Roeb, Schmücker, Sattler, Solar Energy, (2014), (2015).



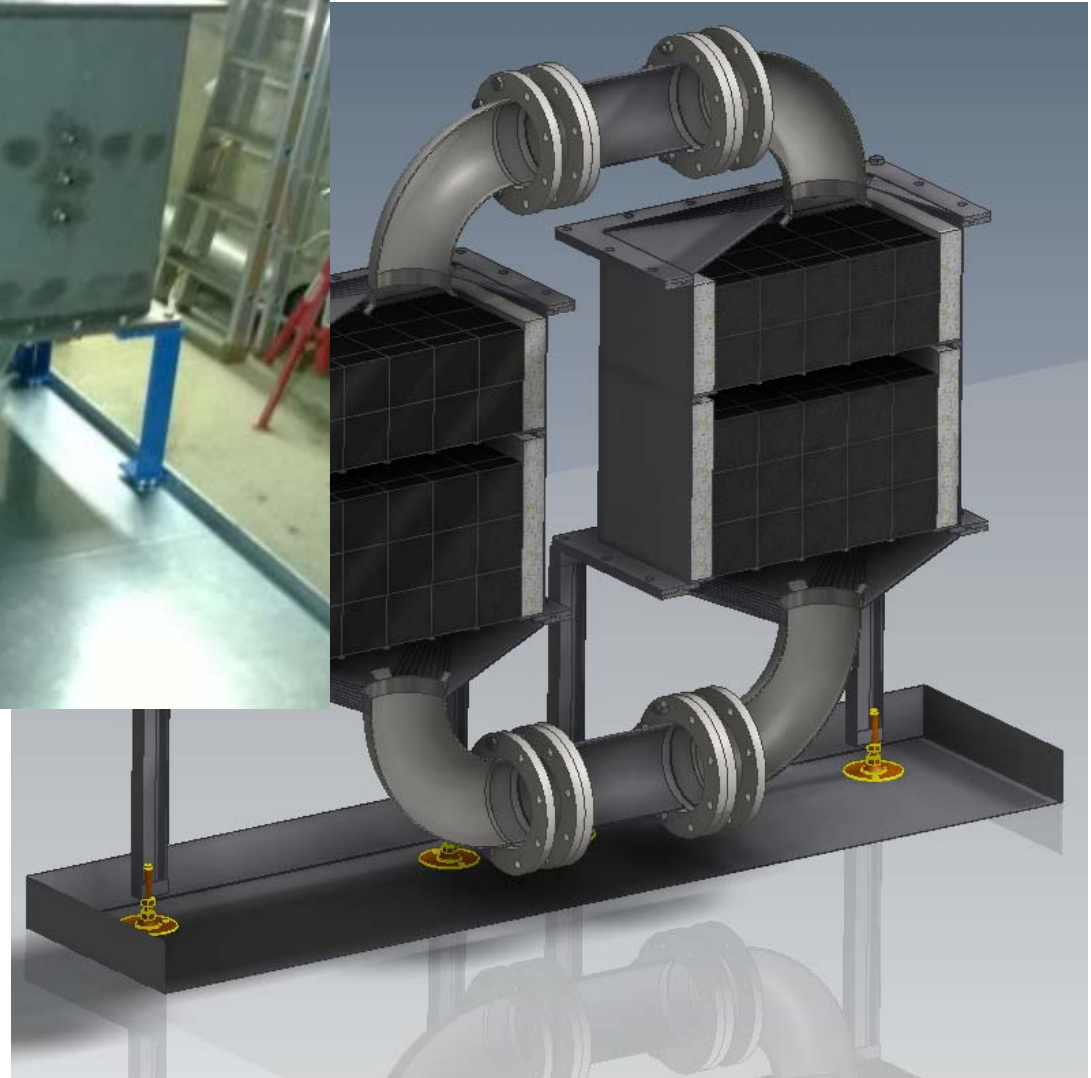
Numerical modelling of the reactor

- gas flow – heat transfer – chemical reaction were modeled
- kinetics model from experimental data was implemented
- predict a cycle
- define the optimal reactor geometry

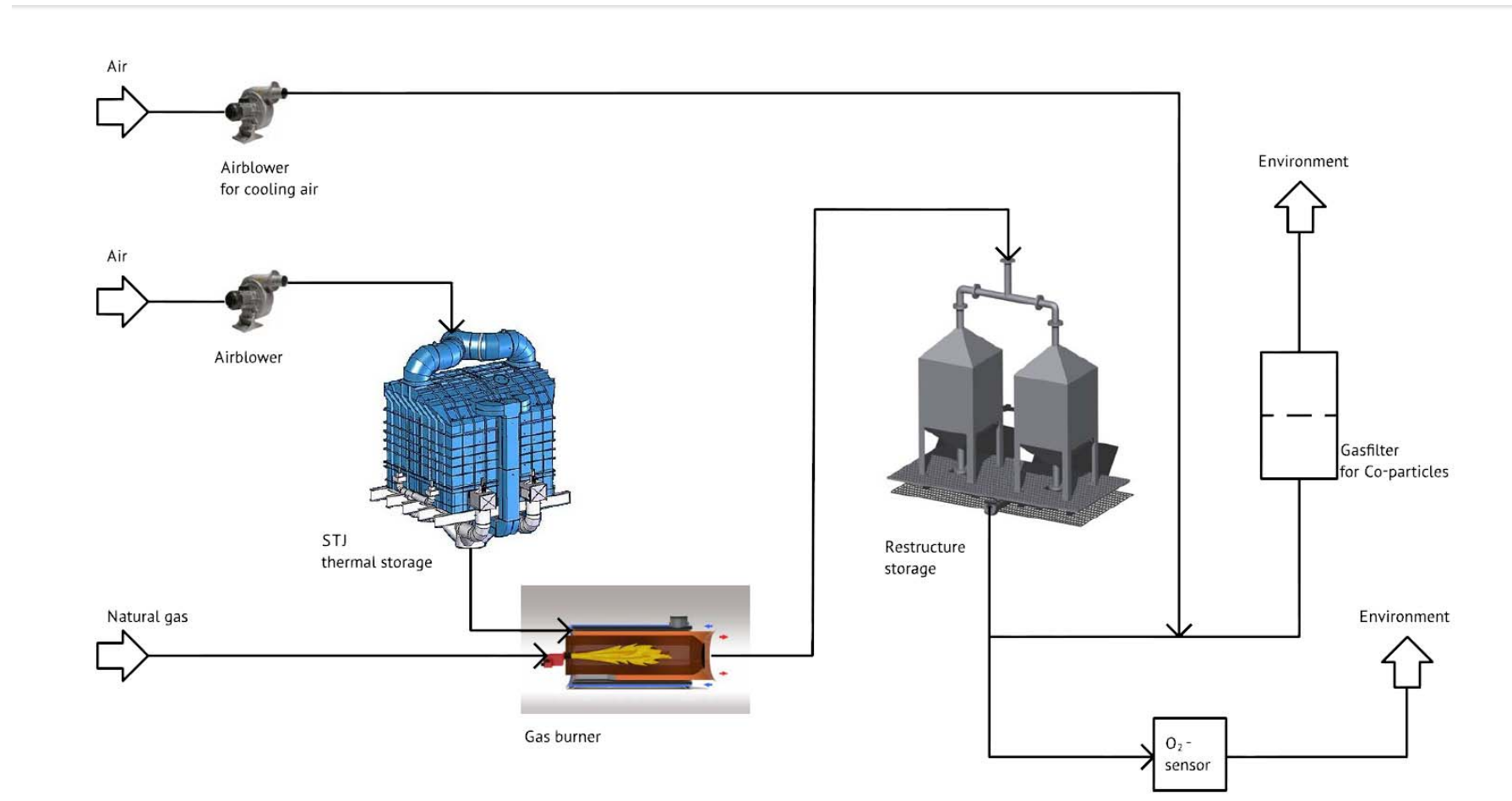


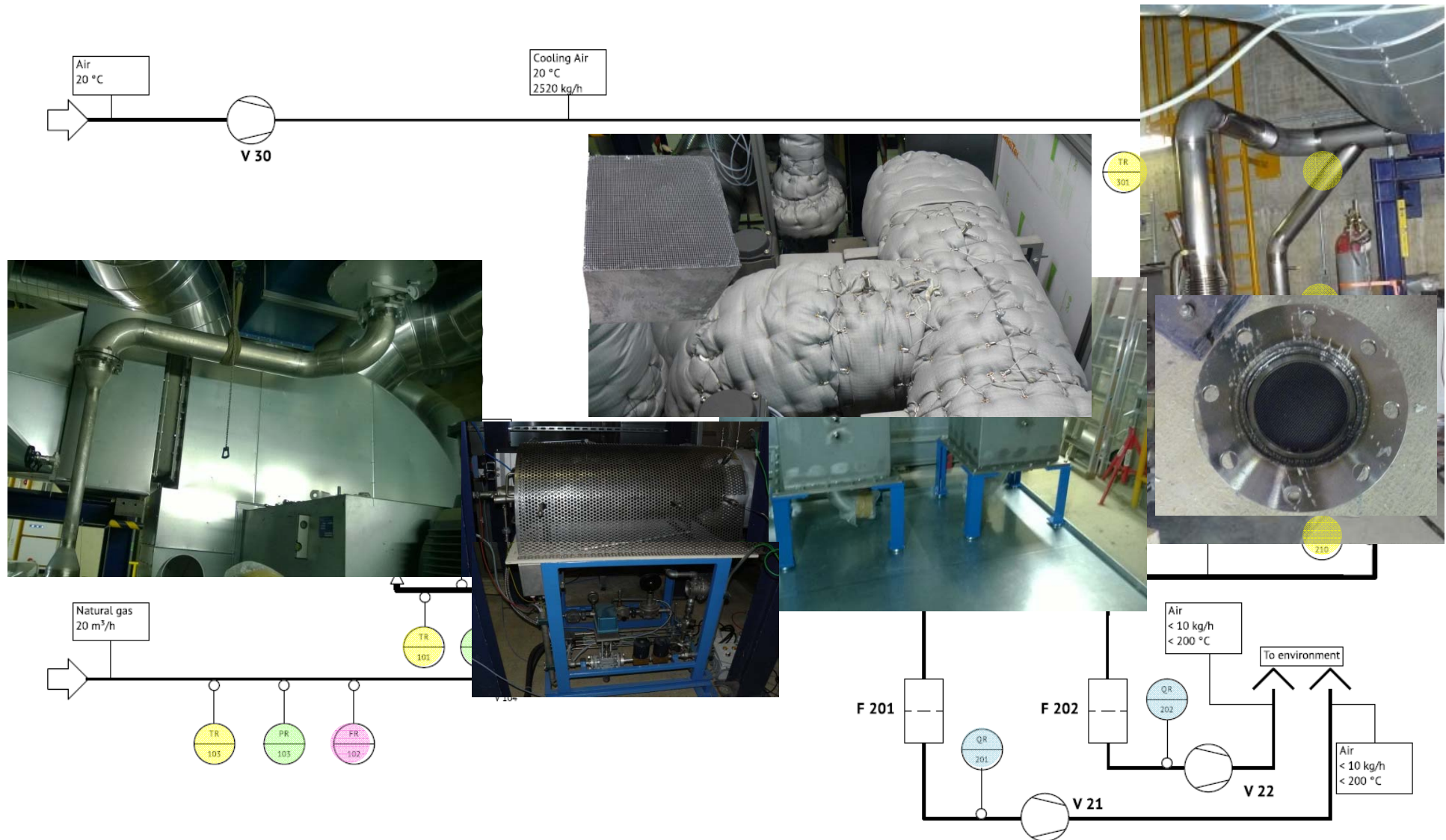


existing solar facility



Implementation in an existing solar facility

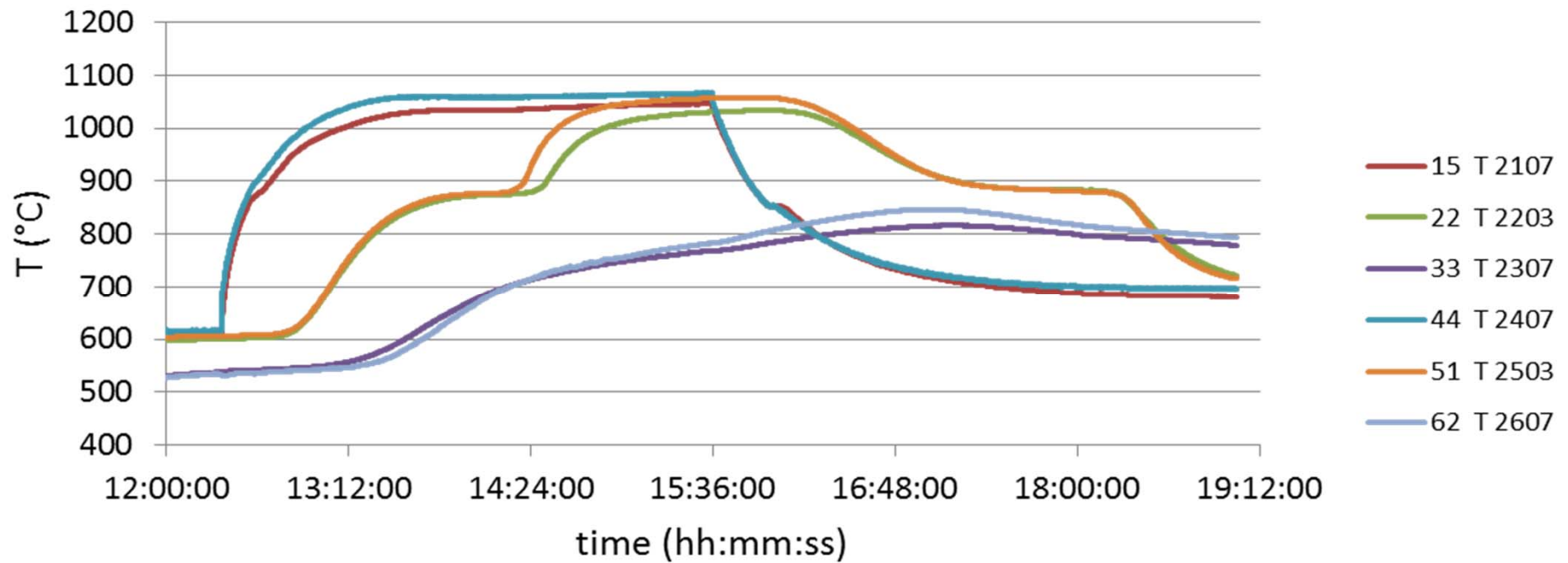




Chemical Tests

evidence of a plateau due to chemical reaction

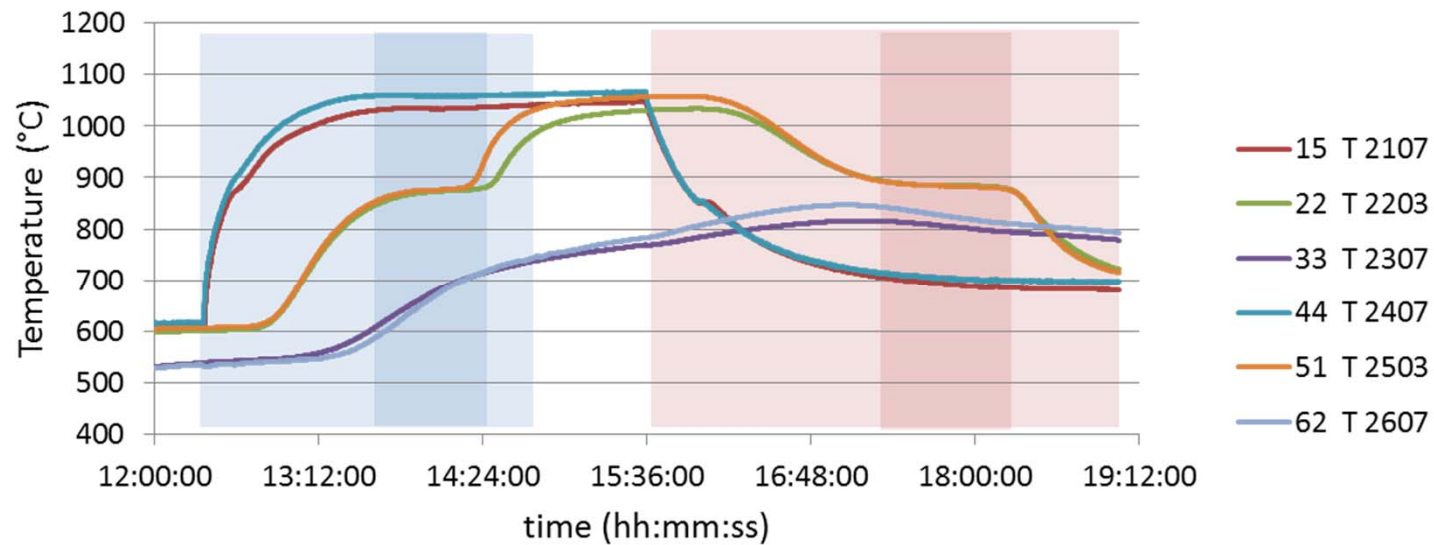
similar behavior of 2 chambers



Chemical Tests

considering half of one chamber ($\approx 25\text{kg}$ cobalt)

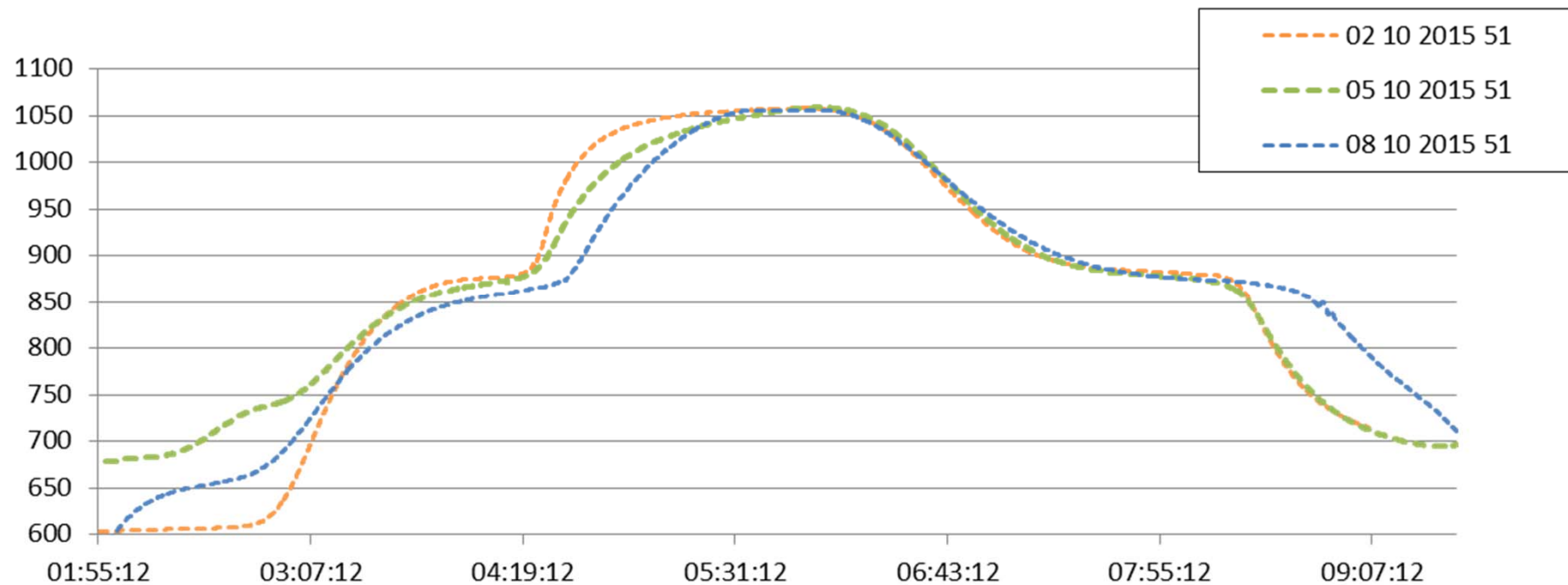
	Energy stored (kWh)	Average Power (kW)	time	at constant temperature
Charge	38	11.2	3.5 h	1 h
Discharge	32	9.6	3.25 h	1 h



Chemical Tests

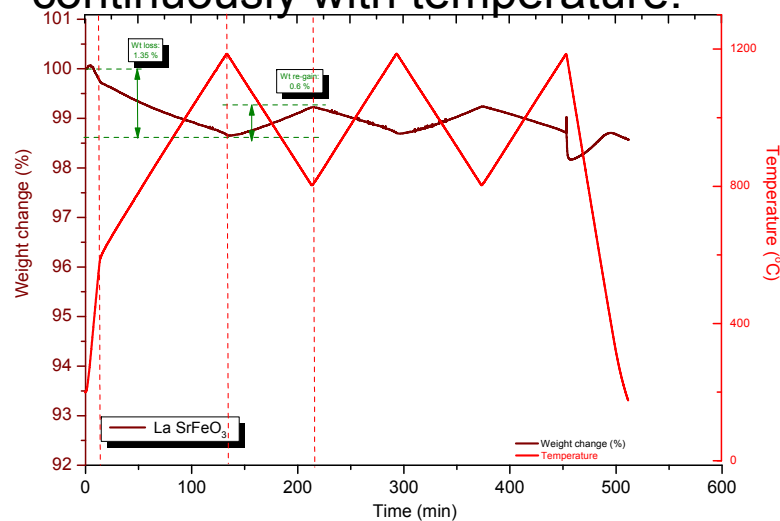
3 complete cycles:

- reproducible results
- material doesn't lose storing capacities in 3 cycles

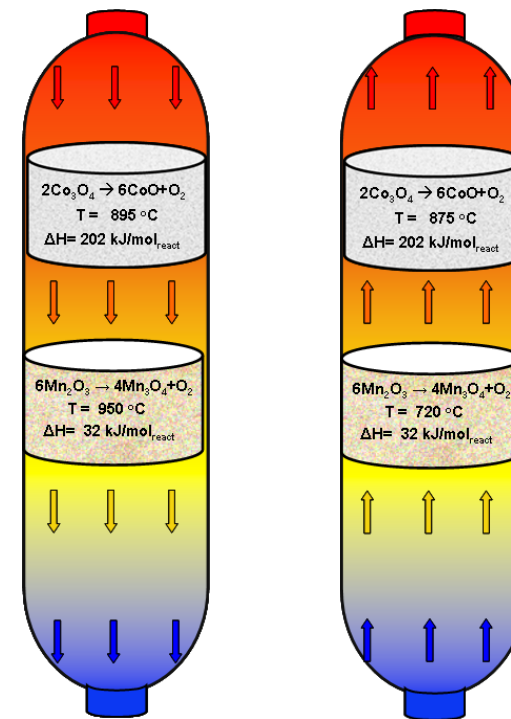


Cascaded ThermoChemical Storage (CTCS)

- CuO/Cu₂O: reduction temperature very close to m.p. of Cu₂O (shrinkage and sintering).
- BaO₂/BaO: BaO reacts with CO₂ present in air to BaCO₃
- Perovskites: loose/gain (little) weight continuously with temperature:



Reaction	ΔH (kJ/mol)	T_{red} (°C)	T_{ox} (°C)
$2 \text{Co}_3\text{O}_4 + \Delta H \rightarrow 6 \text{CoO} + \text{O}_2$	202.5	895	875
$6 \text{Mn}_2\text{O}_3 + \Delta H \rightarrow 4 \text{Mn}_3\text{O}_4 + \text{O}_2$	31.9	950	720

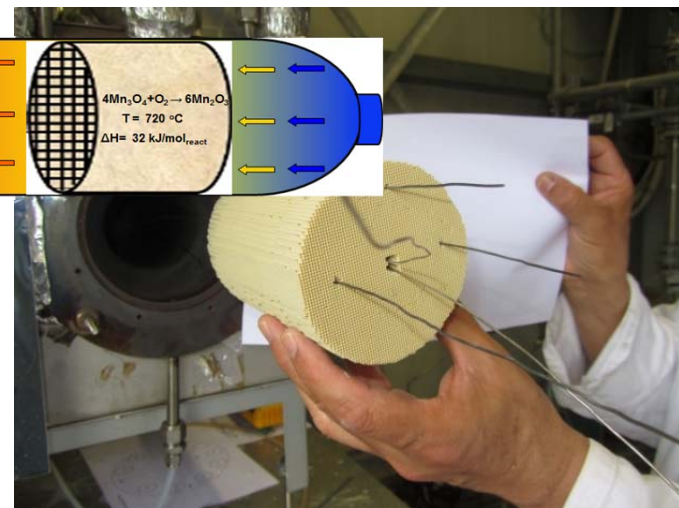
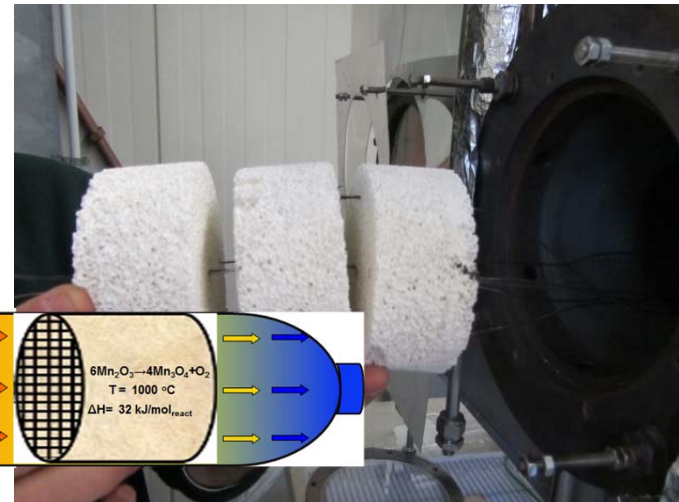
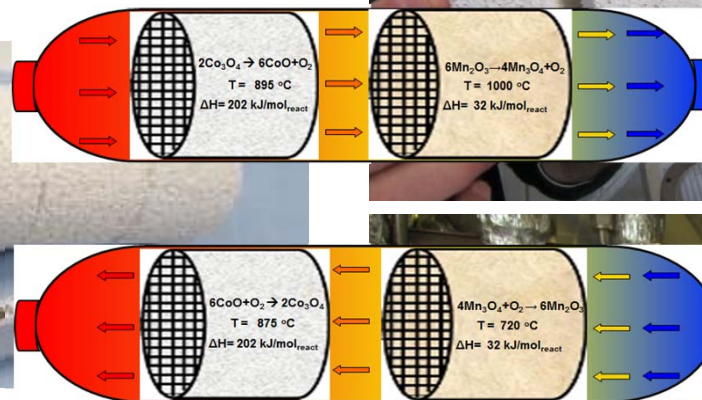
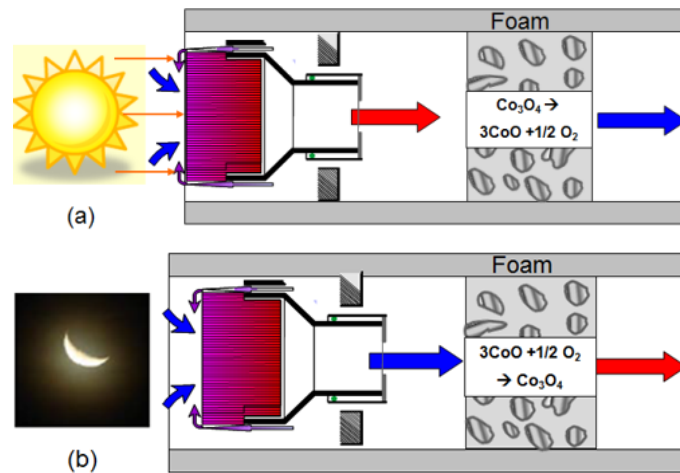


Solar campaigns: comparative testing of two storage module types

• 3 Cordierite foams

30 ppi; BYLIM

Length = 12 cm



• 1 Cordierite honeycomb

400 cpsi; NGK

Length = 12 cm

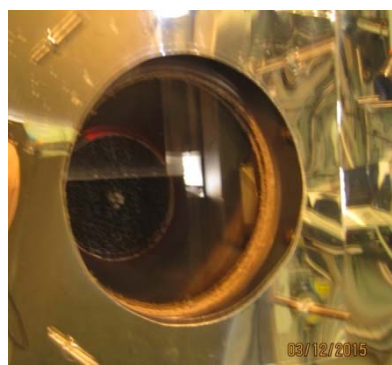


Comparative testing of three SiC receivers (190 slm)

SiSiC honeycomb
90 cpsi; Schunk
Weight ≈ 1404 g
Length = 15 cm



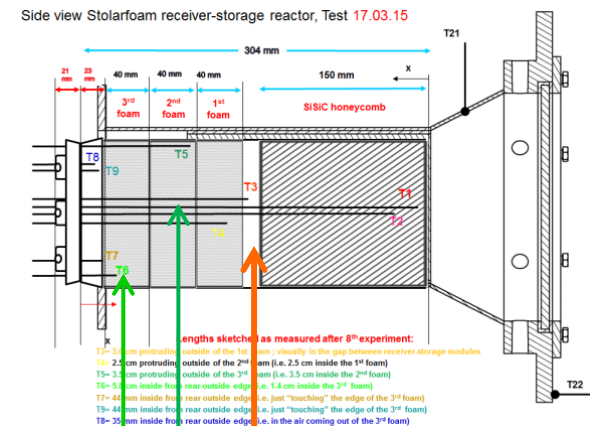
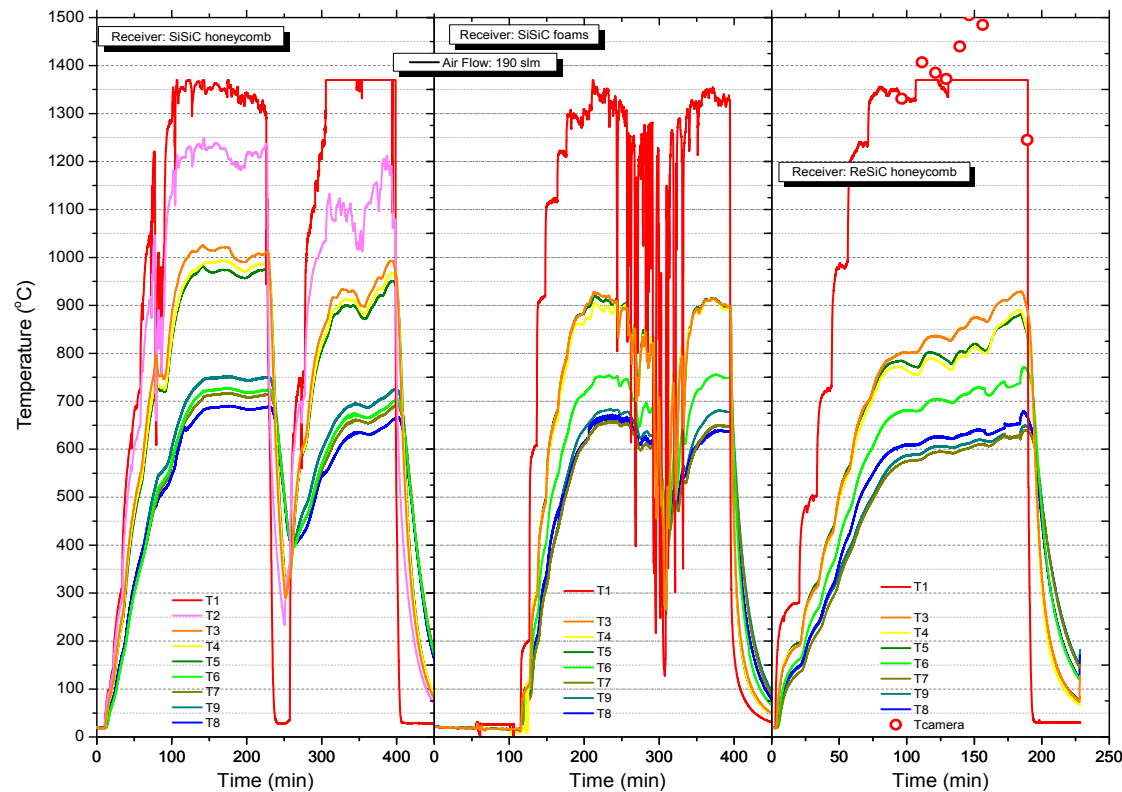
3 SiSiC foams
10 ppi; ERBICOL
Weight ≈ 246 g
Length = 12 cm



ReSiC honeycomb
90 cpsi; Stobbe TC
Weight ≈ 584 g
Length = 10 cm



Comparative performance of SiC receivers tested



T3≈1030°C

T5≈ 975°C

T6≈ 725°C

T3≈930°C

T5≈915°C

T6≈755°C

T3≈930°C

T5≈875°C

T6≈775°C



Solar energy can be stored in elemental sulfur via a three step thermochemical cycle

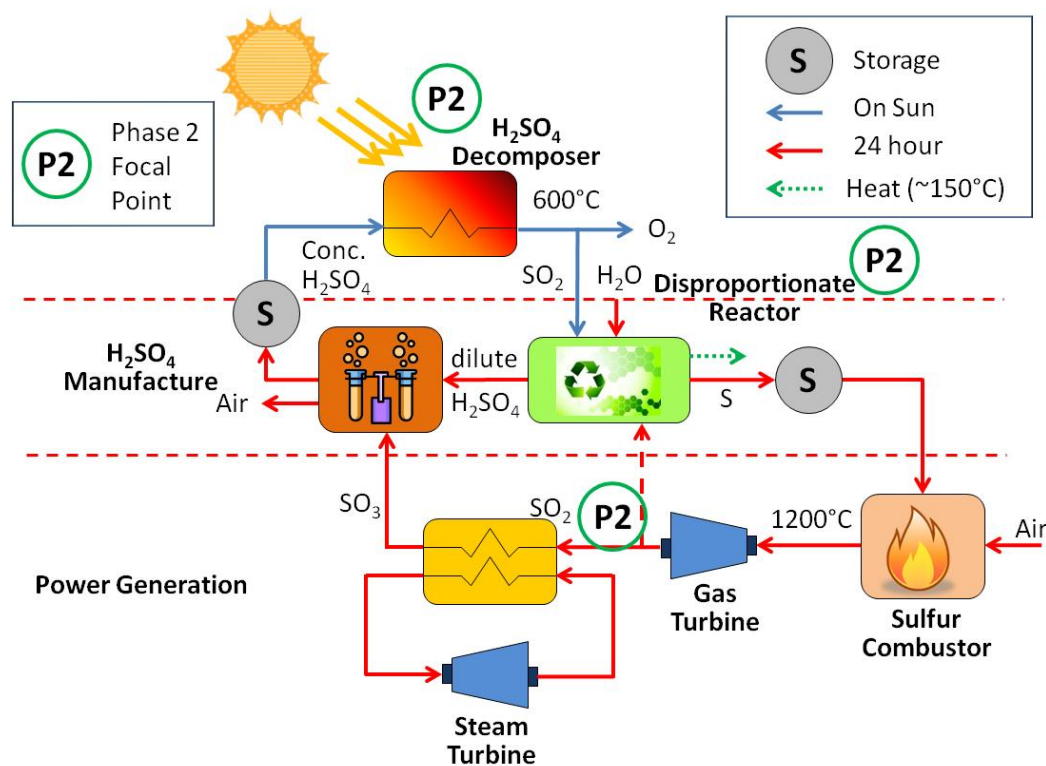


	Reaction	Temp (°C)
H_2SO_4 Decomposition	$2\text{H}_2\text{SO}_4 \rightarrow 2\text{H}_2\text{O}(\text{g}) + \text{O}_2(\text{g}) + 2\text{SO}_2(\text{g})$	800
SO_2 Disproportionation	$2\text{H}_2\text{O}(\text{l}) + 3\text{SO}_2(\text{g}) \rightarrow 2\text{H}_2\text{SO}_4(\text{aq}) + \text{S}(\text{l})$	150
Sulfur Combustion	$\text{S}(\text{s,l}) + \text{O}_2(\text{g}) \rightarrow \text{SO}_2(\text{g})$	1200



An improved flowsheet was established based on modeling and experimental data from Phase I

- Plant design incorporated established processes from sulfuric acid manufacturing plant



DOE Metric	LCOE (¢/kWh _e)
DOE Target	6.5
CSP w/Sulfur Storage	8.1*

*SAM (NREL) using 2012 costs

- Storage cost is < \$2/kWh
- LCOE is ~6¢/kWh_e based on proposed Sunshot targets



Achievements

- Thermochemical storage is an efficient way for the operation of high temperature solar-thermal power plants
- A demonstrator with two times 50 kg CoO is presently tested successfully at the solar tower of DLR in Jülich, Germany
- Cascade Thermochemical Storage will improve such systems
- Sulfur promises to be cost efficient and easy to integrate in existing processes

Outlook

- New materials are necessary as well for the sensible as for the thermochemical storage
- A further scale-up is under preparation



Acknowledgements:

- To **EU** for financing the MARIE CURIE ACTION Intra-European Fellowships (IEF) Call: FP7-PEOPLE-2011-IEF, Grant 300194: Thermochemical Storage of Solar Heat via Advanced Reactors/Heat exchangers based on Ceramic Foams (STOLARFOAM)
- To **EU** for financing the FP7-ENERGY-2011-1 Grant 283015 Redox Materials-based Structured Reactors/Heat Exchangers for Thermo-Chemical Heat Storage Systems in Concentrated Solar Power Plants (RESTRUCTURE)
- To **DoE** for financing Sulfur based thermochemical heat storage for Baseload (DOE Baseload program DE-EE0003588)
- To **DLR** Programmdirektion Energie (PD-E) for funding through Project Thermochemical storage for CSP-applications based on Redox-Reactions – from materials to processes (REDOXSTORE).





Thank you very much for your attention!

